# Single Pellet DP-PSA Experiments for the Characterisation of Heat and Mass Transfer Parameters



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## **Overview of DP-PSA system**



#### Aim

Extract heat and mass transfer information from temperature data of the single pellet DP-PSA system

#### **Experimental system**

 Closed system with two independently controlled pistons:



Figure 1. Dual-Piston Pressure Swing Adsorption (DP-PSA) system. The inset shows the position of the 4 thermocouples inside the column.

- Cycle times from seconds to minutes
- Different pressure ratios and profiles
- Measurements:
  - Absolute pressure and pressure drop
  - Two pairs of thermocouples along the column length
  - In each pair one in the gas phase and one inside a 13X pellet

Figure 2. Schematic showing the DP-PSA system

## **Comparison of the experimental data with simulations**



#### **Pressure profile**

- Pressure profile depends mainly on piston position and thus system volume
- Minor influence of fluid temperature
- Experimental pressure profile agrees with simulated pressure profile



Figure 3. Comparison of the simulated and measured pressure for a helium run. Also shown is the position of the two pistons.

#### **Temperature profile**

- For non-adsorbing gases the fluid temperature depends on the compression and wall heat transfer
- Measured temperature profile lags behind the simulated temperature
- Simulated and measured temperature profiles agree if the thermocouple (TC) response is included

Figure 4. Comparison of the measured and simulated temperature profile for a helium run

### Heat transfer between the fluid and solid phase



#### **Temperature profile**

- The solid lags behind the fluid temperature due to gas/solid heat transfer
- The temperature profile for a fast cycle  $(t_c=2s)$  shows that the thermocouples are responsive enough to capture the



temperature swing in the fluid phase

• The CO<sub>2</sub> runs in Figure 6 show the effect of mass transfer and heat of adsorption on the solid phase temperature

### Conclusion

 Good agreement between the simulated and experimental profiles

 Heat transfer coefficients can be gained from helium runs and mass transfer coefficients from CO<sub>2</sub> runs

Figure 6. Comparison of the experimental fluid phase temperature  $(T_f)$  and solid phase temperature  $(T_s)$  profile for CO<sub>2</sub> runs at different cycle times  $(t_c)$ 

#### References

Acknowledgements

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1. Friedrich, Ferrari, Brandani: Efficient Simulation and Acceleration of Convergence for a Dual Piston Pressure Swing Adsorption System, Industrial & Engineering Chemistry Research, 2013. 2. Dang, Friedrich, Brandani: Characterisation of an automated Dual Piston Pressure Swing Adsorption (DP-PSA) system, Energy Procedia, in press.

Figure 5. Comparison of the experimental

fluid phase temperature  $(T_f)$  and solid

phase temperature  $(T_s)$  profile for helium

runs at different cycle times (t<sub>c</sub>)